

DOE's EGS Program Review

Using CO₂ as Working Fluid in EGS to Combine Energy Extraction with Sequestration of Carbon

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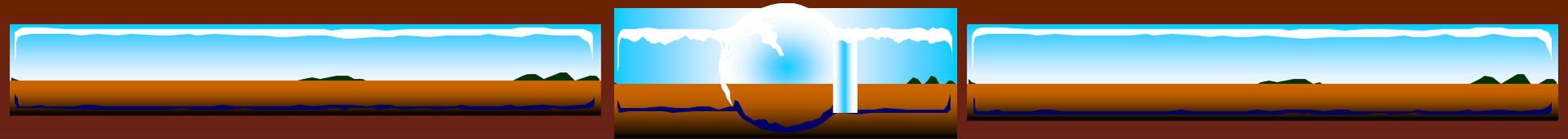
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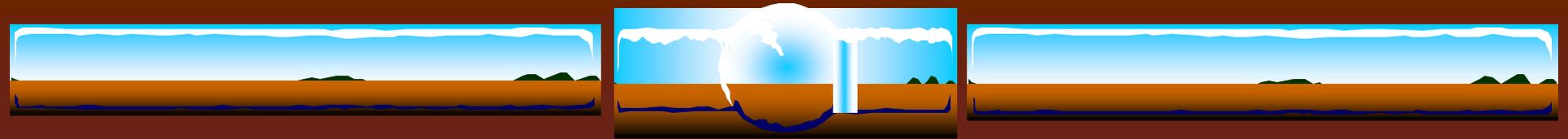
Marriott Hotel
Golden, CO



Project Objective

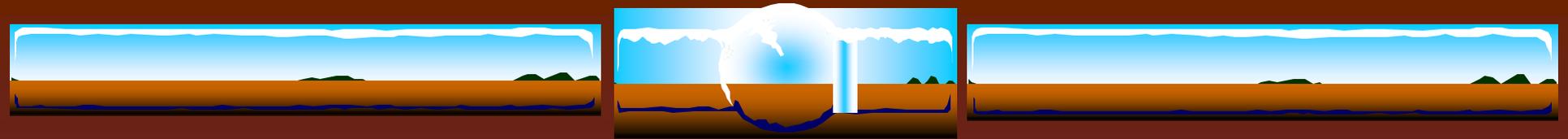
Evaluate the feasibility of using CO₂ as heat transmission fluid for EGS, and compare with “conventional” water-based systems. Assess the potential for combining energy extraction with sequestration of CO₂.

Change: CO₂-based EGS represents a new initiative in our project on “Geothermal Reservoir Dynamics.” This has grown to a major priority in our FY06 work that had not been anticipated in earlier planning.



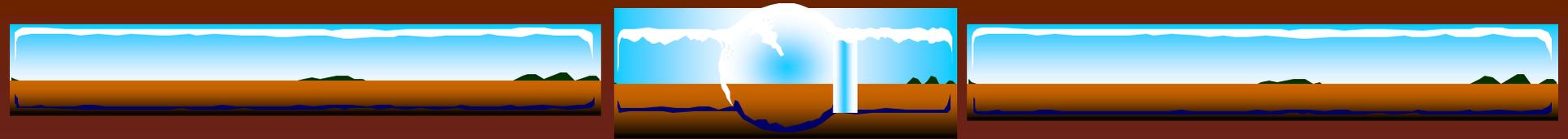
Challenges and Opportunities for EGS

- ❖ Water is a powerful solvent for many rock minerals, making it very difficult to achieve long-term stable operation of water-based EGS systems.
- ❖ Inevitable water losses may seriously impede the viability of EGS in water-short regions, such as the Western U.S.
- ❖ Using CO₂ as heat transmission fluid may avoid the chemistry problems of water-based systems, may offer competitive or superior performance as a working fluid for heat extraction, and may allow to achieve CO₂ sequestration as an ancillary benefit.
- ❖ Operating EGS with CO₂ offers a game-changing alternative, with large potential for superior performance and improved economics.



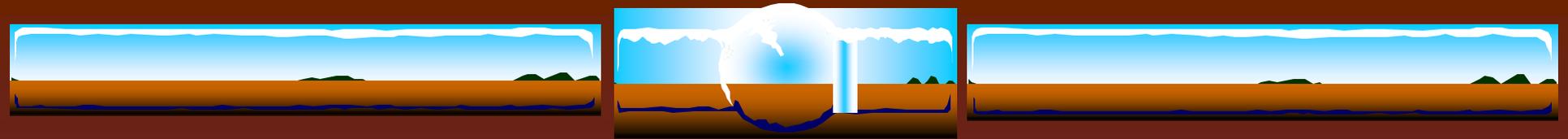
Background/Approach

- ❖ The concept of using CO₂ as working fluid for EGS was originally proposed by Donald Brown (2000), but has received little attention in the technical community.
- ❖ Our modeling capabilities have matured to the point where we could begin a serious quantitative evaluation of the relative merits of water and CO₂ as heat transmission fluids for EGS.
- ❖ LBNL staff active in geothermal research has leveraged their strong engagement in studies of CO₂ storage in geologic formations.
- ❖ Initial studies showed such enormous promise for CO₂ that much of our EGS effort planned for FY06 was redirected towards EGS-CO₂.



Results/Accomplishments

- ❖ Presented a first paper on our findings at the Stanford 2006 geothermal workshop.
- ❖ Assisted DOE in developing a White Paper to support the case for an EGS-CO₂ R&D programme.
- ❖ Submitted a paper with detailed reservoir engineering analyses of CO₂-based EGS to *Geothermics*.
- ❖ Submitted an abstract on EGS-CO₂ to the GSA Annual Meeting (Philadelphia, October 2006).

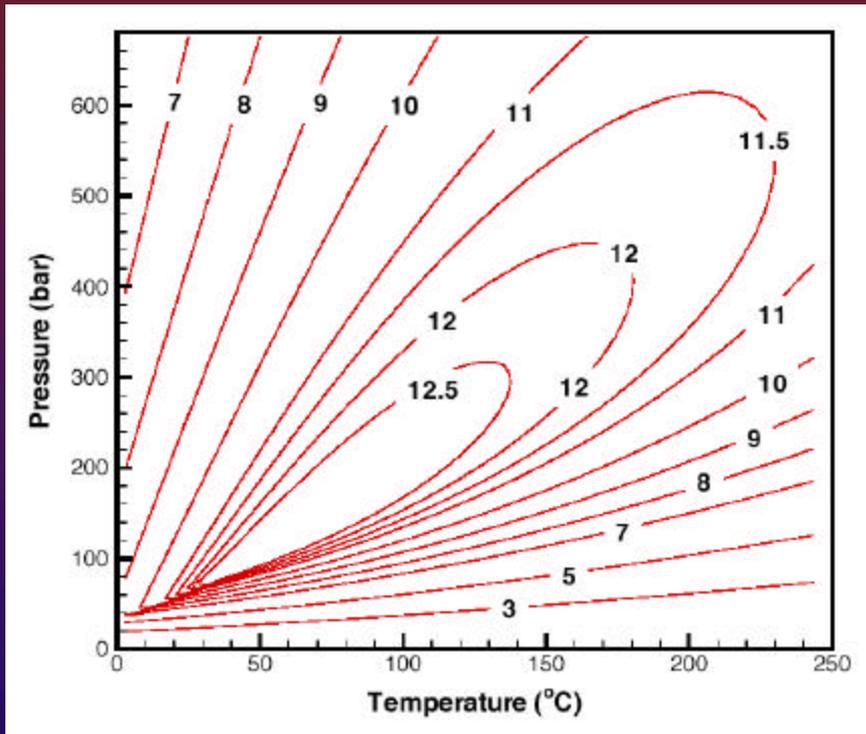


CO₂ and Water Compared as Heat Transmission Fluids for EGS

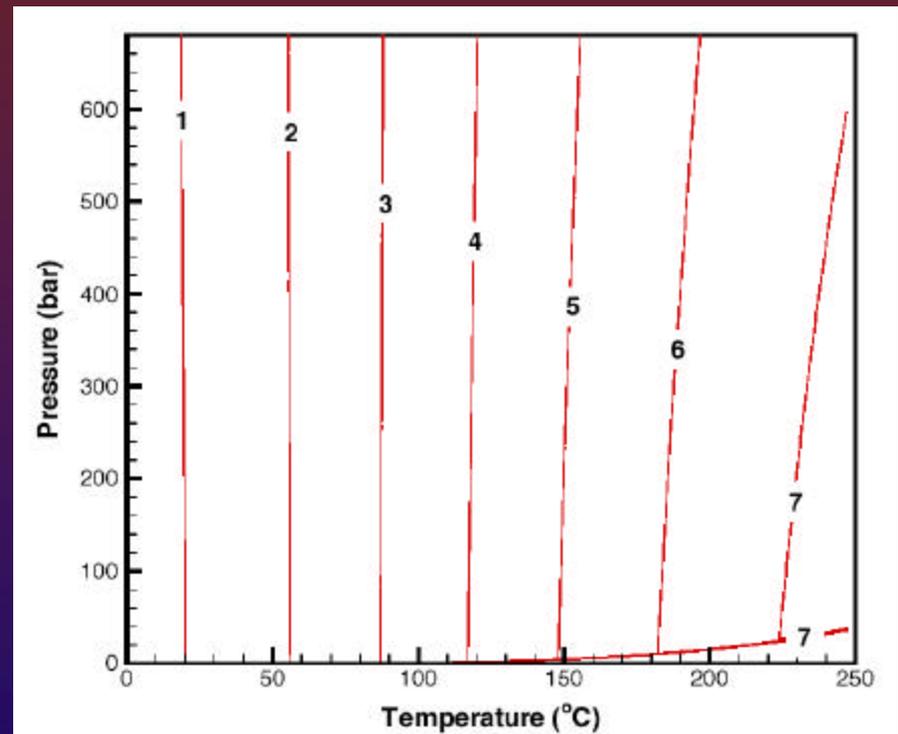
property	CO ₂	water
ease of flow	lower viscosity , lower density	higher viscosity, higher density
heat transmission	smaller specific heat	larger specific heat
fluid circulation in wellbores	highly compressible and larger expansivity ==> more buoyancy	low compressibility, modest expansivity ==> less buoyancy
fluid losses	earn credits for storing greenhouse gases	costly
chemistry	poor solvent; significant upside potential for porosity enhancement and reservoir growth	powerful solvent for rock minerals: lots of potential for dissolution and precipitation



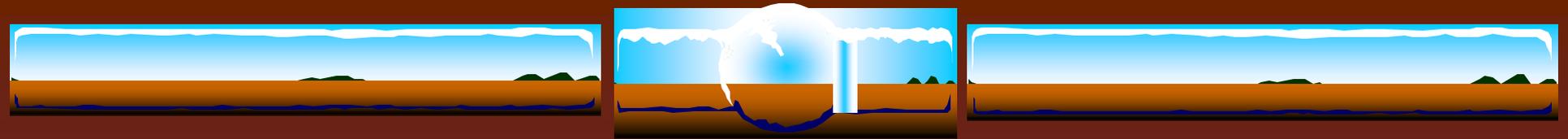
Ratio of Fluid Density to Viscosity (10^6 sm^{-2})



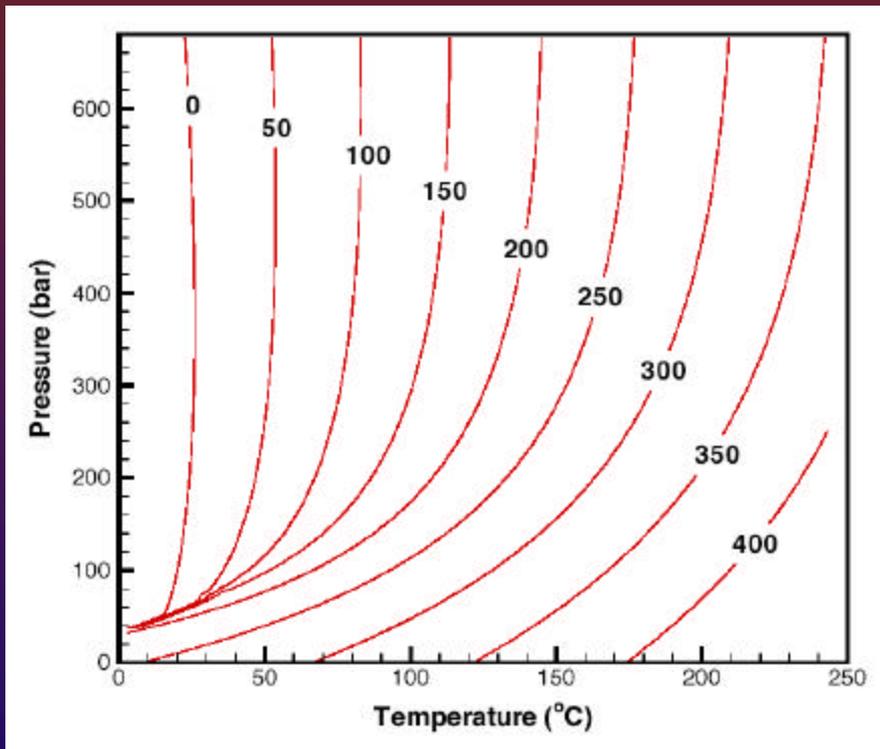
CO₂



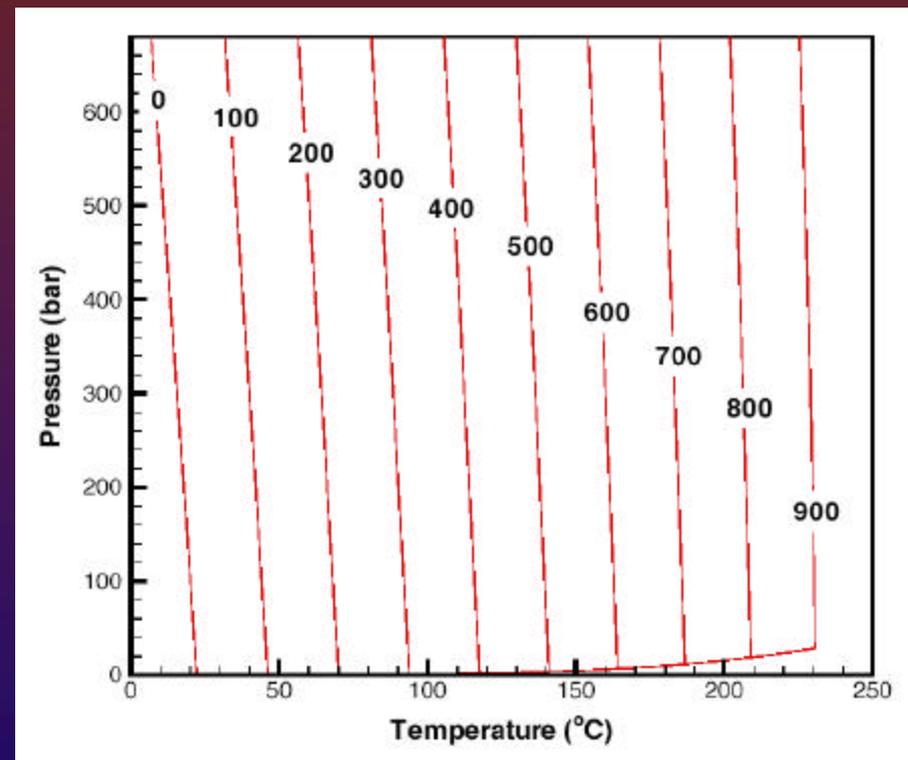
water



Specific Enthalpy (kJ/kg)

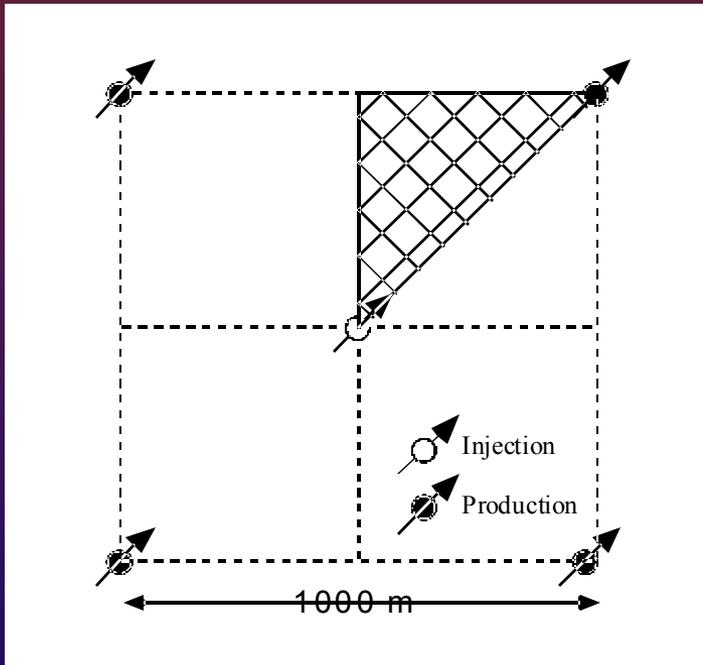


CO₂



water

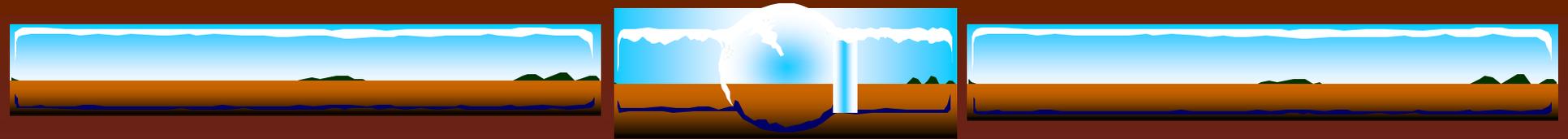
Five-Spot Well Pattern for Heat Extraction Studies



Formation	
thickness	305 m
fracture spacing	50 m
permeable volume fraction	2%
permeability	$50.0 \times 10^{-15} \text{ m}^2$
porosity in permeable domain*	50%
rock grain density	2650 kg/m^3
rock specific heat	$1000 \text{ J/kg/}^\circ\text{C}$
rock thermal conductivity	$2.1 \text{ W/m/}^\circ\text{C}$
Initial Conditions	
reservoir fluid	all CO_2 , or all water
temperature	200°C
pressure	500 bar
Production/Injection	
pattern area	1 km^2
injector-producer distance	707.1 m
injection temperature	20°C
injection pressure (downhole)	510 bar
production pressure (downhole)	490 bar

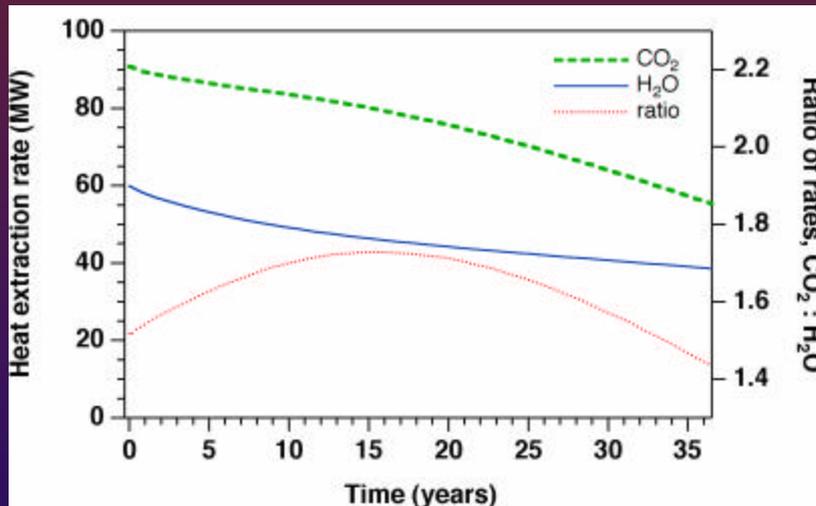
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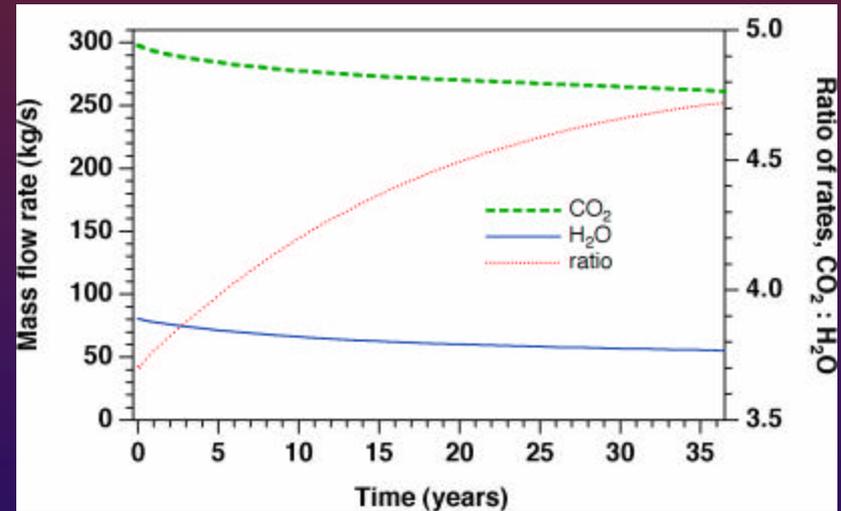


Results for Reference Case

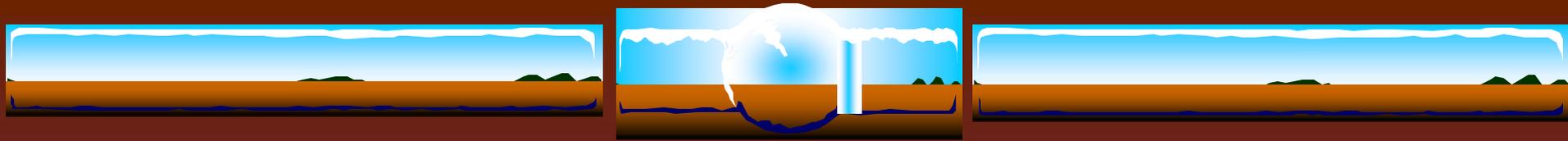
$$T_{\text{res}} = 200 \text{ }^\circ\text{C}, P_{\text{res}} = 500 \text{ bar}, T_{\text{inj}} = 20 \text{ }^\circ\text{C}$$



Heat extraction rate

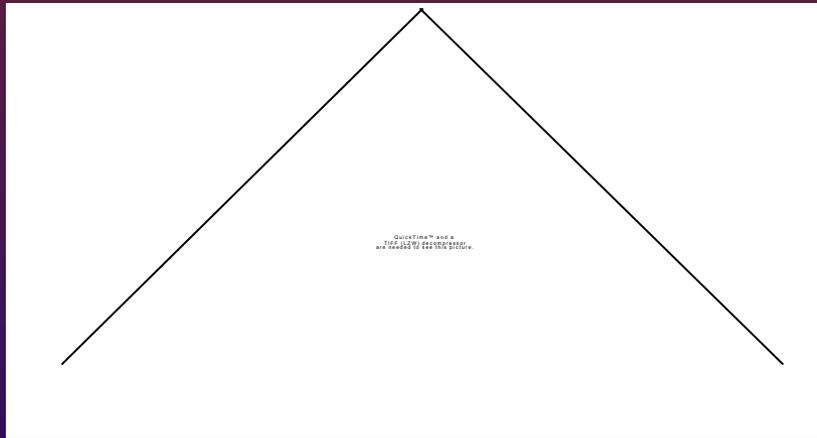


Mass flow rate

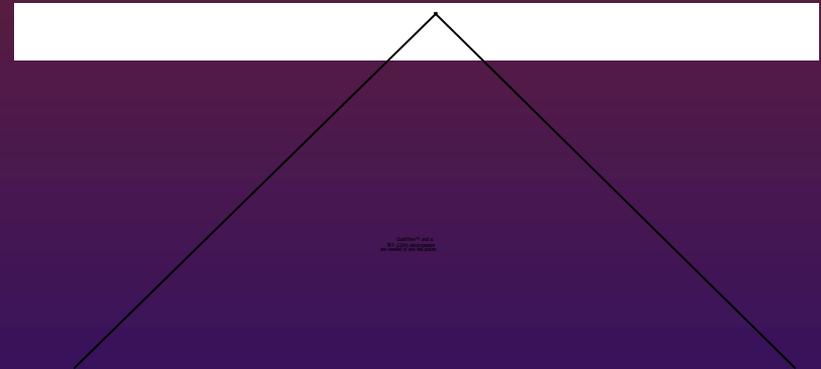


Reference Case - Temperatures after 25 Years

$$T_{\text{res}} = 200 \text{ }^\circ\text{C}, P_{\text{res}} = 500 \text{ bar}, T_{\text{inj}} = 20 \text{ }^\circ\text{C}$$



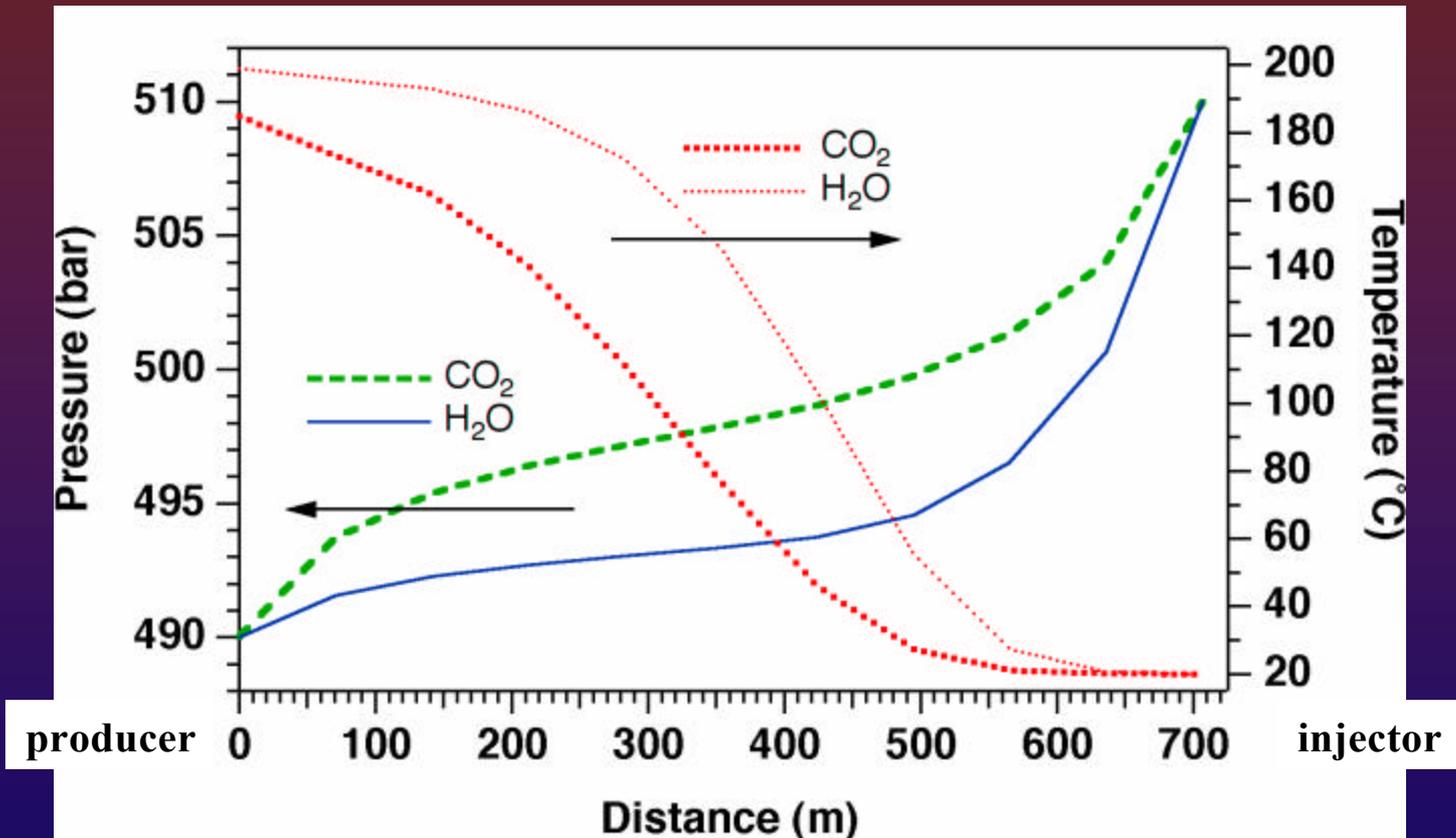
CO₂



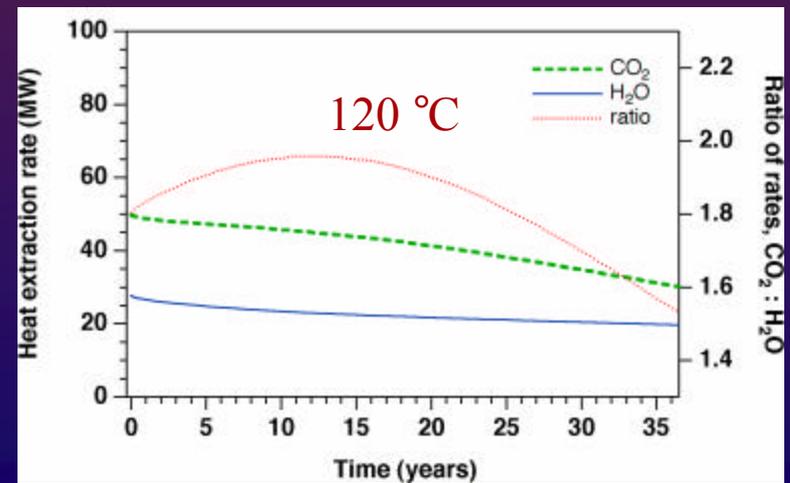
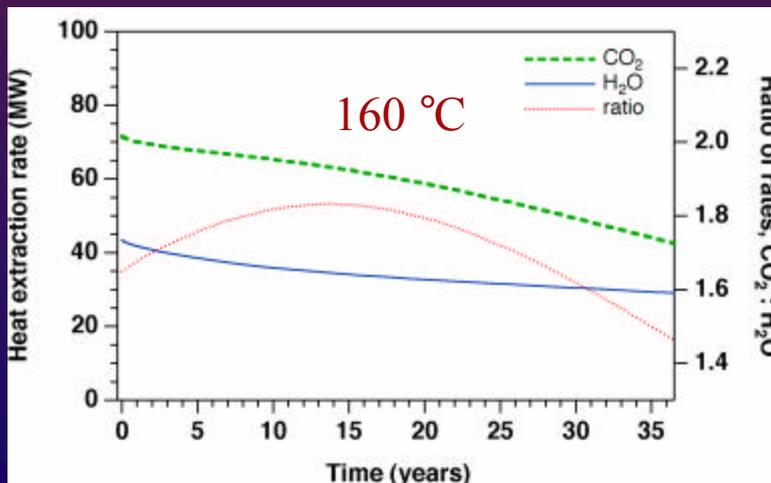
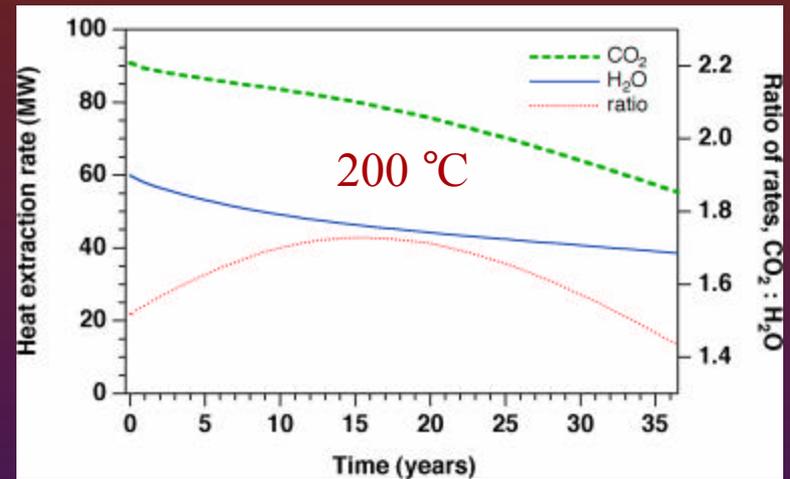
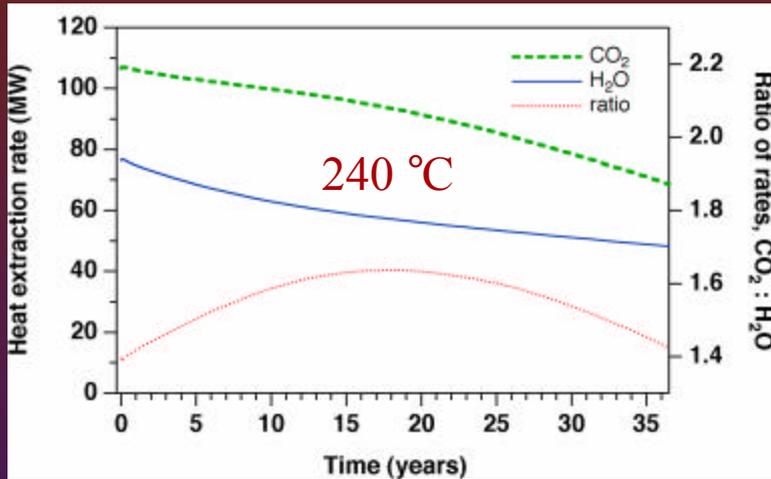
water

Reference Case after 25 Years

Profiles along a Line from Producer to Injector



Different Reservoir Temperatures

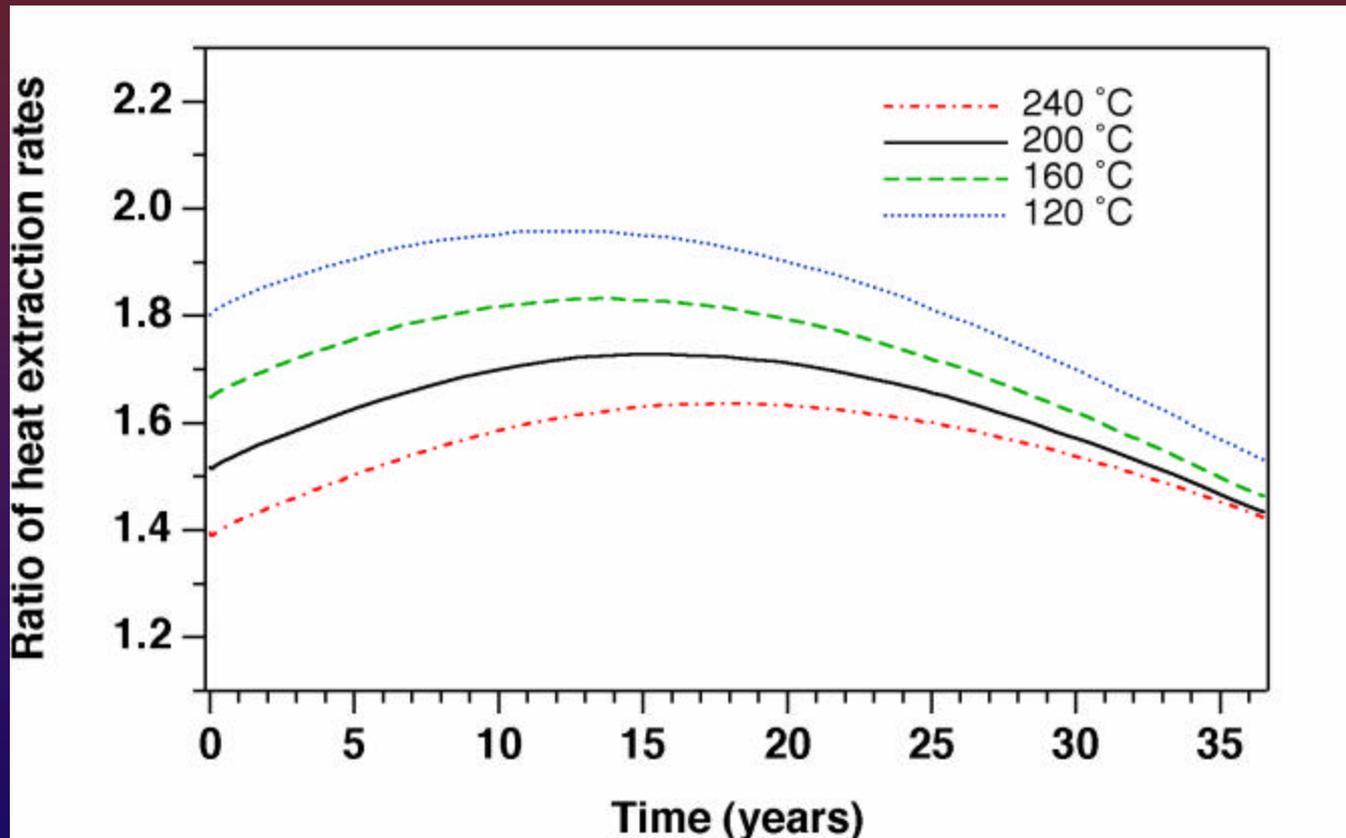


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CO₂ vs. Water Heat Extraction Rates

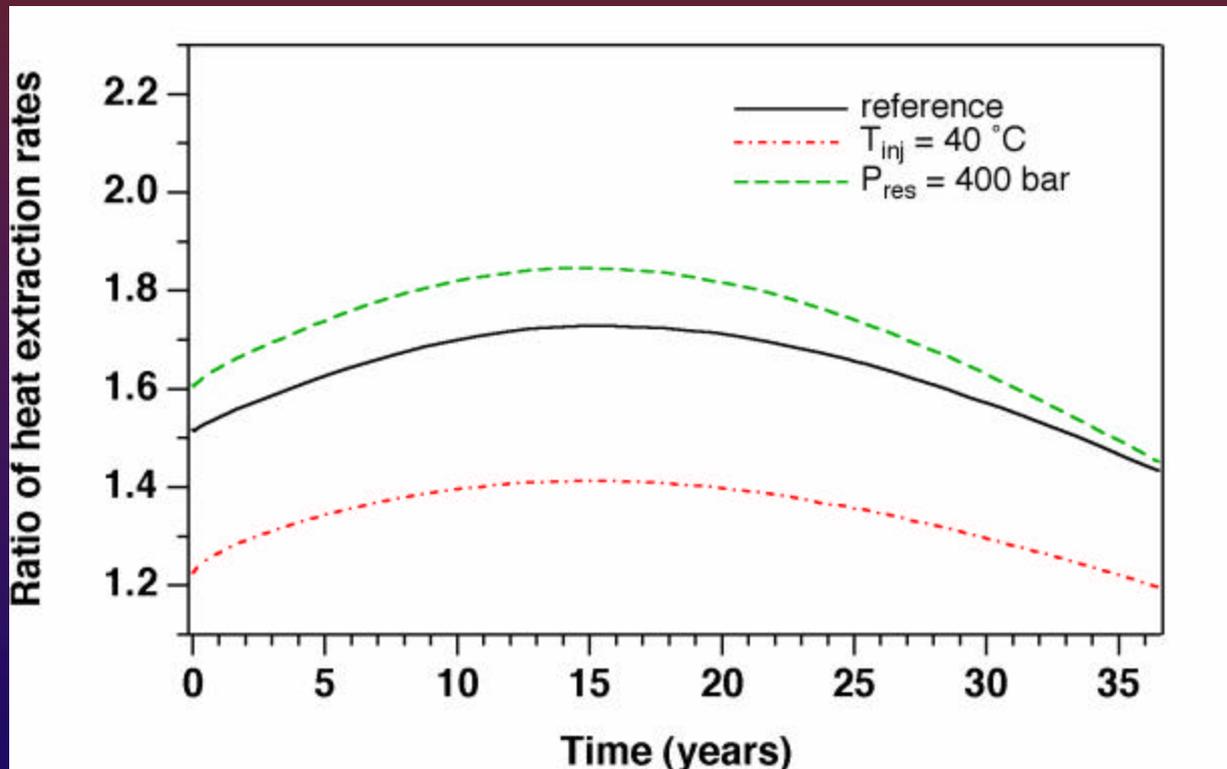
Different Reservoir Temperatures



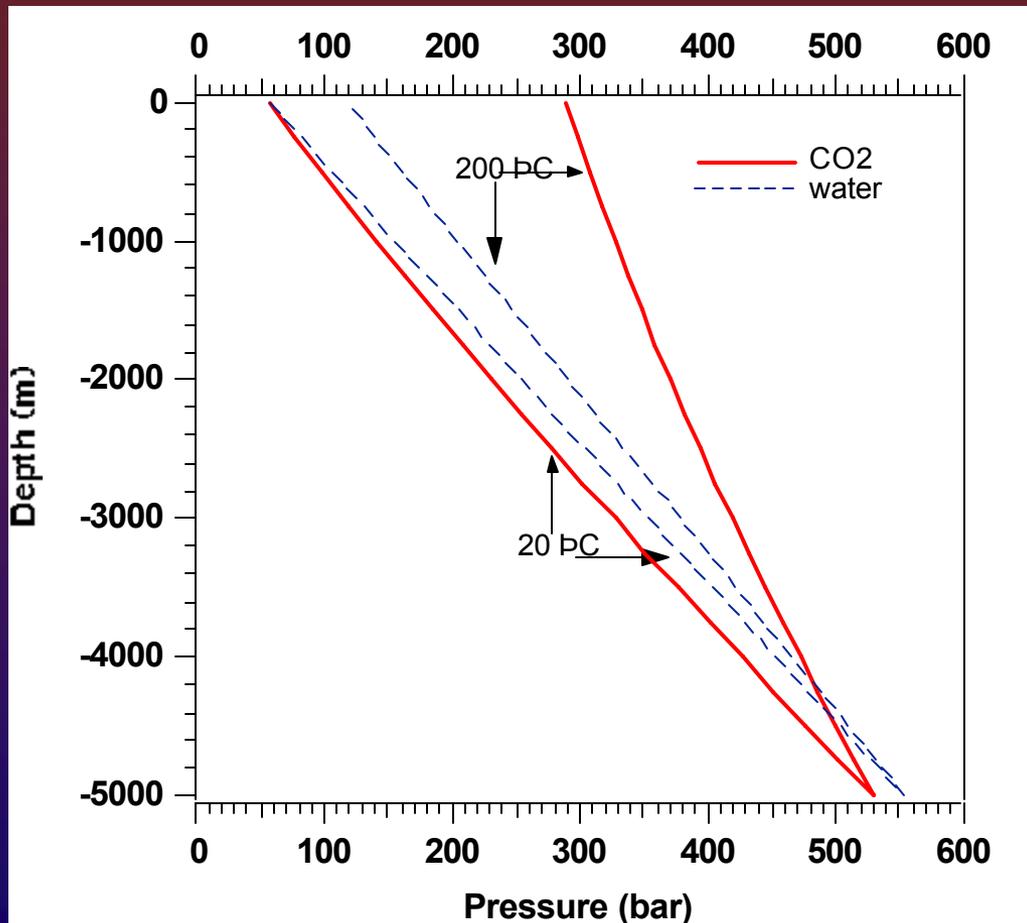


CO₂ vs. Water Heat Extraction Rates

Dependence on Injection Temperature and Reservoir Pressure



Wellbore Flow: CO₂ vs. Water



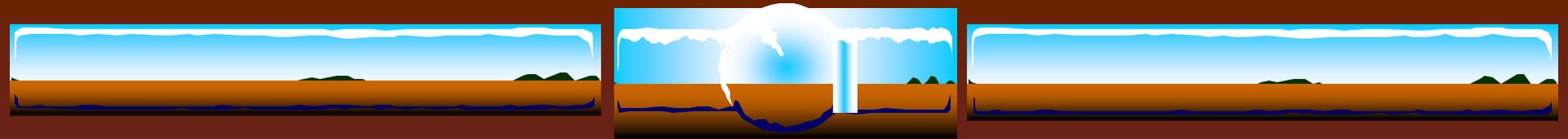
$$? P = P_{\text{prod}} - P_{\text{inj}}$$

$$\text{CO}_2: 288.1 - 57.4 = 230.7 \text{ bar}$$

$$\text{Water: } 118.6 - 57.4 = 61.2 \text{ bar}$$

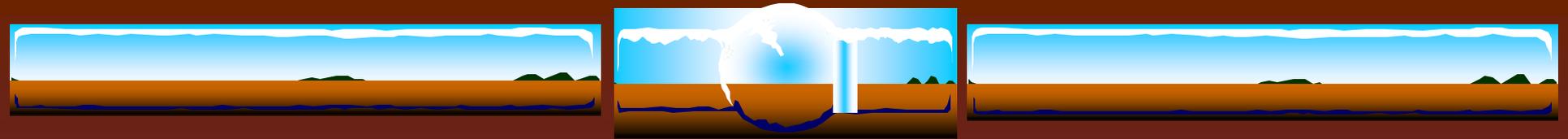
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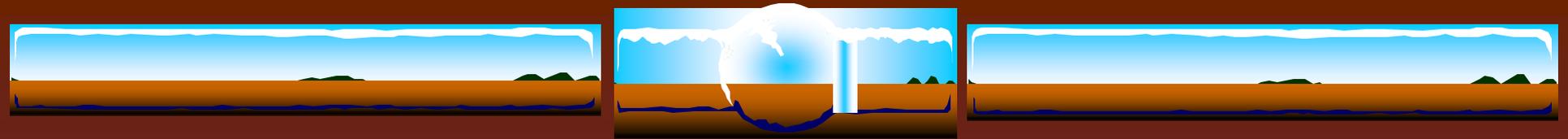
CO₂ Storage Capacity

- ❖ Mathematical modeling suggests that a CO₂ mass flow of approximately 20 kg/s is required per MW electric power capacity.
- ❖ From experience with long-term circulation tests with water-based systems, expect a fluid loss rate of order 5%, or 1 kg/s of CO₂ per MW electric power.
- ❖ For 1,000 MWe of installed EGS capacity, the amount of fluid lost in circulation and stored underground is estimated as 1 tonne of CO₂ per second.
- ❖ This rate of fluid storage is equivalent to CO₂ emissions from 3,000 MWe of coal-fired power generation.
- ❖ CO₂ inventory in 1,000 MWe of installed EGS capacity is estimated as 137 Mt.



Summary of Results

- ❖ Thermophysical properties make CO₂ an attractive fluid for heat extraction.
- ❖ Heat extraction rates when using CO₂ are estimated to be approximately 50 % larger than for water.
- ❖ Larger buoyancy forces compared to water mean reduced power requirements for the fluid circulation system.
- ❖ Chemical interactions between rocks and fluids would be weaker and are likely to be more favorable for CO₂ than for water.
- ❖ Unavoidable fluid losses are costly for water, but could earn greenhouse gas storage credits when using CO₂. The sequestration potential for EGS-CO₂ is large.
- ❖ It may be possible to feed CO₂ directly to the turbines, obviating the need for a heat exchanger and secondary fluid circulation.



Conclusion

- ❖ Will the project objective be achieved by the project completion date?
 - ❖ Yes – initial demonstration of attractive properties of CO₂ as heat transmission fluid has already been achieved.
 - ❖ No – project is just getting started, no completion date has been set.